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Thermochimica Acta 436 (2005) 35–42

thermochimica acta

www.elsevier.com/locate/tca

# Solventless fingerprinting of bituminous materials: A high-resolution thermogravimetric method

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Received 19 April 2005; received in revised form 13 June 2005; accepted 20 June 2005 Available online 10 August 2005

## **Abstract**

The thermogravimetry (TG) of bituminous materials by means of a constant heat rate is often plagued by low resolution and poor reproducibility of the degradation or mass loss temperatures. The TG curve, or the associated differential TG (DTG) signal, is thus an unreliable quality control or quality assurance (QC/QA) method. A 2- and 3-step high-resolution TG/DTG method was developed for these materials for analysis between 150 and 800 ◦C. The DTG results, obtained within 2 h, show about 10 discrete mass loss peaks, the profile being material dependent. The reproducibility of the results indicates that the methods may be used for rapid QC/QA and material fingerprinting. The development of the method is detailed and its application is illustrated with the analysis of several bitumens and polymer-modified bituminous sealants.

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*Keywords:* Bitumen; Asphalt; Analysis; Thermogravimetry; TG; DTG; High-resolution; Quality control; Quality assurance; QC/QA; Fingerprinting

## **1. Introduction**

Bitumen is the basis of products that find numerous applications in civil engineering, including water-borne coatings, roadway binders, and polymer-modified bituminous waterproofing membranes and sealants. For the industrial production of materials with consistent properties, it is often desirable to use raw materials of a constant composition or grade; however, products of identical grades can have different compositions [1], as indicated in Table 1. A constant chemical composition may be required for some applications, an important one being the production of stable bitumen–polymer mixtures [2].

The comp[ositi](#page-7-0)on of bitumen i[s](#page-1-0) [often](#page-1-0) [co](#page-1-0)ntrolled by means of chromatography (for various methods, see Table 1 in [3]). This approach requires the separation of bitumen into several fractions. T[he](#page-7-0) [co](#page-7-0)mposition as indicated in Table 1, for instance, is unique and serves to control the identity of a raw material. It is a fingerprint tedious [to](#page-1-0) [obtain](#page-1-0), [howe](#page-7-0)ver, and it requires that several organic solvents be used and later discarded.

In contrast to chromatography, thermogravimetry (TG)/ differential TG (DTG) is a solventless method. In standard TG, a sample is heated at a constant rate. The method, which provides information about thermal stability and weight loss with rising temperature, has long been used to characterize petroleum products [4,5]. Despite some success, the method shows poor resolution and reproducibility, especially in the  $350-450$  °C region, where uncontrolled combustion (autoignition) occurs [6]. Fig. 1 shows an example with bitumen duplicate[s.](#page-7-0) [Due](#page-7-0) to poor reproducibility, the DTG profile has not permitted successful fingerprinting of bitumen [7]. Alternative methods used to overcome this difficulty have consi[sted](#page-7-0) [of](#page-1-0) [the](#page-1-0) [m](#page-1-0)easurement of weight loss at fixed temperatures, e.g. 2 min at 350, 500 and 750 °C [8], and the quantification of the heaviest bitumen fractio[n](#page-7-0) [afte](#page-7-0)r heating at rapid rates [9].

In this paper, it is shown that a 3-step high-resolution TG/DTG method can be used to i[mpro](#page-7-0)ve both the resolution and the reproducibility of the results to a level that all[ows](#page-7-0) for rapid quality control/quality assurance (QC/QA)

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<sup>0040-6031/\$ –</sup> see front matter © 2005 Published by Elsevier B.V. doi:10.1016/j.tca.2005.06.025

<span id="page-1-0"></span>Table 1 Composition in percent wt of PG58-28 bitumens from different sources<sup>a</sup>

Bitumen source	$AAA-1$ Lloydminster	$AAK-2$ Boscan	AAS-2 Arab heavy
<b>Saturates</b>	11	8	
Naphtene aromatics	32	31	46
Polar aromatics	37	39	30
Asphaltenes $(n$ -heptane)	16	19	

 $a$  From [1].



Fig. 1. DTG results from duplicate runs on bitumen heated at  $20^{\circ}$ C/min.

and true fingerprinting of bituminous products at all temperatures between 150 and 800 ◦C. Fig. 2 shows an example of the type of improvement that can be obtained. The aim of this paper is to show how such improvements were made possible and to describe some applications of the method by showing results for bitumens and bituminous sealants. It is best, however, to begin with a brief review of the basis for TG/DTG where samples are not heated at a constant rate. To be concise, the following abbreviations are used in this review: d*p*/d*t*, rate of pressure change; d*m*/d*t*, rate of mass loss; d*T*/d*t*, heat rate; d*T*/d*t*(max), maximum heat rate; d*T*/d*t*(min), minimum heat rate; *R*, resolution setting; and *S*, sensitivity setting.



Fig. 2. Standard and high-resolution DTG for bitumen (dotted curve was shifted up for improved clarity).

## **2. Varying rate thermogravimetric analysis**

## *2.1. Early methods*

To increase the resolution of TG over what is possible with a linear rate of heating, Rouquerol [10,11] and Paulik and Paulik [12,13] independently developed the idea of using the thermal characteristics of the sample to control its heat rate and achieve quasi-equilibrium conditions. Under such conditions, a predetermined te[mperature](#page-7-0) program no longer exists. [Meth](#page-7-0)ods based on this guiding principle have received close to 20 names over time [11]. In the current state of the technology, the thermal characteristics are not limited to mass, but also include length, heat flow and evolved gas flow [11]. In TG, the sample mass is monitored.

To achie[ve a no](#page-7-0)n-linear heat rate, Rouquerol [10] evacuated a sample bulb linked to a pressure gauge connected to a temperature controller. As the sample [was](#page-7-0) [h](#page-7-0)eated and the vapour pressure increased, the heating was reduced. The effect was thermal decompositio[n](#page-7-0) [at](#page-7-0) [a](#page-7-0) constant rate. With the use of an electro-balance and feedback loop, Paulik and Paulik [12] demonstrated that a linear heat rate  $(0.5-5 \degree C/\text{min})$  could be reduced when a weight loss was detected. The result was a very slow heat rate, i.e. quasiisothermal conditions that led to sample decomposition rates in the ra[nge](#page-7-0) [o](#page-7-0)f 0.1–0.5%/min [13].

Rouquerol [11] and Paulik and Paulik [13] obtained very slow heat rates by measuring d*p*/d*t* and d*m*/d*t*, respectively. In such quasi-equilibrium conditions, sample decomposition occurs within a nar[row tem](#page-7-0)perature interval, which improves res[olution](#page-7-0). Sorensen later dev[eloped](#page-7-0) a similar control [14], whereupon a sample was heated at a constant rate until a predetermined rate of mass change was detected. The isotherm was then held until the mass loss rate dropped below another predetermined threshold. This approach, us[eful fo](#page-7-0)r measuring decomposition kinetics, is known as stepwise isothermal analysis [15,16].

#### *2.2. Control algorithms*

[The](#page-7-0) increase in resolution that follows a reduced rate of heating comes at the expense of experimental time. To shorten experimental times while maintaining high resolution, Crowe and Sauerbruun developed algorithms [17,18] that amongst other things, allow for very high heat rates, e.g. >50  $\mathrm{C/min}$ , while avoiding overshoot of the temperature where mass loss occurs. One algorithm provides for two experimental methods: the dynamic rate and t[he](#page-7-0) [consta](#page-7-0)nt decomposition rate. Both of these methods were used in this work, consequently details about the methods are warranted.

#### *2.2.1. Dynamic rate*

With this method, d*T*/d*t* is continuously tuned to d*m*/d*t* such that d*T*/d*t* approaches a set maximum when d*m*/d*t* is small, and d*T*/d*t* tends to zero when d*m*/d*t* is large. As expected, the lower is d*T*/d*t*, the longer is the experimental

<span id="page-2-0"></span>Table 2 Effect of *R* on d*T*/d*t* (min) in dynamic rate experiments at specific d*T*/d*t* (max)

R	$dT/dt$ (max) (°C/min) <sup>a</sup>					% of dT/dt
	50	20	10	5		
	10.02	4.01	2.00	1.00	0.20	20.03
2	3.68	1.47	0.74	0.37	0.07	7.37
3	1.36	0.54	0.27	0.14	0.03	2.71
4	0.50	0.20	0.10	0.05	0.01	1.00
5	0.18	0.07	0.04	0.02	0.01	0.37
6	0.07	0.03	0.01	0.01	0.01	0.13
7	0.02	0.01	0.01	0.01	0.01	0.05
8	0.01	0.01	0.01	0.01	0.01	0.02

<sup>a</sup> Experimental limit is 0.01 ◦C/min.

time. It is thus left to the experimentalist to select the minimum allowed d*T*/d*t* based on the input of a resolution factor  $(R)$  and the maximum heat rate, with  $0.1 \le R \le 8$ . The minimum allowed rate is calculated as [18]:

$$
\frac{dT}{dt}(\text{min}) = 0.001 \, \exp(6.3 - R) \, \frac{dT}{dt}(\text{max})
$$

The allowed d*T*/d*t* (min) is [thus](#page-7-0) reduced by a lower d*T*/d*t* (max) and a rising *R*. The range between d*T*/d*t* (max) and d*T*/d*t* (min) during the heating of a sample can be fairly wide. With d*T*/d*t* (max) at 50 ◦C/min and *R*-values of 1 and 7, for example, d*T*/d*t* (min) is 10.02 and 0.02 ◦C/min, respectively (Table 2). For any given heat rate, the minimum allowed rate may be expressed as a percentage of the maximum heat rate for any given *R* (Table 2). The effect of *R* in the analysis of bitumen, for example, is well demonstrated in Fig. 3. As *R* increases, the response to a change in mass loss is faster and the allowed d*T*/d*t* (min) is reduced.

With any *R*-value, the algorithm allows for the difference between d*T*/d*t* (max) and d*T*/d*t* (min) to be reduced with a sensitivity setting (*S*), which varies from 1 to 8. The default value of  $S = 1$  admits the full range of heat rates. Values of 2 and 3 reduce this range to about 50% and 30%, and higher *S*-values reduce it further [19]. The effect of *S* is most easily understood by looking at the heat rate curves in Fig. 4. Below



Fig. 3. Effect of *R* on d*T*/d*t* in a dynamic rate experiment applied to bitumen.



Fig. 4. Effect of *S* on d*T*/d*t* in a dynamic rate experiment applied to bitumen.

350 ◦C, a rising *S* provides for faster heating before a mass loss is detected and a faster drop in d*T*/d*t* once it is detected. After a mass loss, a rising *S* also leads to a more rapid increase in  $d/dt$ , e.g. beyond 500 °C in Fig. 4. Consequently, a rise in *S* provides for conditions increasingly close to stepwise isothermal heating.

## *2.2.2. Constant decomposition rate*

The other experimental approach provided by the algorithms of Crowe and Sauerbruun [17,18] allows for maintaining a heat rate such that sample decomposition occurs at a constant rate. In this case, the d*T*/d*t* (max) is typically set at 5 ◦C/min in the absence of mass loss and possible *R*values vary from −0.1 to −[8,](#page-7-0) [an](#page-7-0)d *S*-values vary from 1 to 8. When a mass loss is measured, the d*T*/d*t* varies so that d*m*/d*t* is constant until no more mass loss is detected. The value of this constant is set through *R*. Table 3 shows some values for *R* and the associated d*m*/d*t* in percent weight loss per min [19]: the lower the value of *R*, the lower the allowed sample decomposition rate and the longer the experimental time.

In the case of a reactive material where oxidation and [dec](#page-7-0)omposition may be rapid, *S* > 1 may help in increasing the resolution of the mass loss temperatures. An increase in *S* in the constant reaction rate experiment lowers the d*m*/d*t* threshold that will bring about a decrease in d*T*/d*t*, thus minimizing a possible overshoot of the decomposition temperature [19].

Table 3

Resolution settings and associated mass loss rates in the [constan](#page-7-0)t decomposition rate experiment

R	$dm/dt$ (%/min)
$-1$	10.000
$-2$	3.160
$-3$ $-4$ $-5$ $-6$ $-7$	1.000
	0.316
	0.100
	0.032
	0.010
$-8$	0.003

<span id="page-3-0"></span>

Fig. 5. Effect of *S* on d*T*/d*t* in a constant rate reaction experiment applied to bitumen.

Increase in *S* may thus lead to cooling as most clearly illustrated for  $S = 3$  near 375 and 475 °C in Fig. 5.

# **3. Experimental**

# *3.1. Materials*

Six bitumens and three polymer-modified bituminous sealants were used. One bitumen was an 85/100 penetration grade product from Petro-Canada. It served to develop the method. The other bitumens were obtained from the Materials Reference Library (MRL) of the Strategic Highway Research Program (SHRP) in the USA. They served to highlight the fingerprinting capability of the method. The bitumens were selected for their performance grade (PG) and for the difference in the origin of the crude oils from which they were obtained. Bitumens AAA, AAK and AAS were graded PG58- 28, whereas bitumens AAG and AAM were, respectively, graded PG58-10 and PG64-16 [1].

The bituminous sealants A, D, and E were amongst several used before [20–22]. They contained a styrene–butadiene type copolymer and a filler, most often calcium carbonate [20].

# *3.2. [Methods](#page-7-0)*

Masses of about 5 mg, unless otherwise indicated, were heated in a Q500 thermogravimetic analyzer from TA Instruments. The samples were heated in an air flow of 60 mL/min, the suggested flow rate for this instrument. The heating conditions were controlled via the Advantage software for the Q Series, v2.0. For standard TG, the linear heat rates were: 1, 5, 10 and 20 $\degree$ C/min. In the varying heat rate experiments, the inputs were the resolution and sensitivity settings, and the maximum heat rate. In the dynamic heat rate experiments, the maximum rate was  $50^{\circ}$ C/min. In the constant rate experiments, the maximum heat rate was 5 ◦C/min. The results were analyzed with a Universal Analysis 2000 software, v3.9a from TA Instruments.

# **4. Results and discussion**

# *4.1. Standard thermogravimetry*

For the benefit of comparison, bitumen was first analyzed by means of standard TG, in which the sample is heated at a constant rate. Fig. 6 shows results for rates of 1, 5, 10 and  $20^{\circ}$ C/min. The DTG profile generally shows three regions or peaks typical of heavy hydrocarbon mixtures [7,23,24]. At  $20^{\circ}$ C/min, for instance, a broad first peak of low intensity shows a maximum near  $350^{\circ}$ C; the most intense peak shows a maximum near  $530^{\circ}$ C; and between these limits is a series of poorly resolved and overlap[ping peaks](#page-7-0). The first peak has been attributed to the distillation of low molecular weight material, and the others to thermal cracking and the loss of volatile fragments [24]. When it is resolved, the highest temperature peak has been used to quantify heavy bitumen fractions [4,9].

Fig. 6 shows that a reduction in the linear heat rate leads to a greater resolution [of](#page-7-0) [the](#page-7-0) low molecular weight material as it moves down in temperature, but it also leads to an increasingly p[oor](#page-7-0) [res](#page-7-0)olution of the other peaks. Consequently, it is difficult to get a proper resolution of all the peaks with standard TG.

## *4.2. Dynamic rates*

The Petro-Canada bitumen was first analyzed in a series of experiments during which the effects of the *R* and *S* settings on the resolution of the various mass losses as seen on the DTG curve were compared. *S* and *R* were, respectively, varied from 1 to 5, and 2 to 6. The effect of some of these settings on the heat rate was shown earlier in Figs. 3 and 4. DTG results for  $S = 1$  and  $R = 2-6$  are shown in Fig. 7. For convenience, the first mass loss peak, which showed as a broad peak of low intensity, was labeled "light fraction", the last mass loss peak was labeled "heavy fr[action", and the](#page-2-0) group of mass losses between the light and he[avy fract](#page-4-0)ions, was called the "middle fraction", as initially illustrated in Fig. 2.



Fig. 6. Standard DTG on bitumen after heating at different rates. All the curves, except the bottom one, were shifted up for improved clarity.

<span id="page-4-0"></span>

Fig. 7. Effect of *R* on the bitumen DTG profile after a dynamic rate experiment.



Fig. 9. Effect of *S* on the bitumen DTG profile after a dynamic rate experiment.

With  $R = 2$  and 6, experimental times were, respectively, 20 min and ∼6h(Fig. 7), in accordance with the effect of *R* on  $d/dt$  (Table 2). With  $R = 1$  (not shown) or 2, the DTG was much like standard TG after heating at  $20^{\circ}$ C/min (Fig. 6). As *R* increased, the light fraction shifted to lower temperatures and resolved itself from the middle fraction starting at  $R = 4$ . [In](#page-2-0) [contr](#page-2-0)ast, the heavy fraction was best resolved from the middle frac[t](#page-3-0)ion with  $R \leq 4$ . Hence, with  $S = 1$  $S = 1$  $S = 1$ , the separation of the light, middle and heavy fractions was best with  $R = 3$ or 4.

Building on the results with  $R=3$  and 4, the effect of an increase in *S* was investigated. With  $R = 3$  and  $S = 1, 3$ , and 5, the light fraction showed as a broad peak centered near 325 °C, whereas the heavy fraction showed as a sharp and intense peak above  $500\,^{\circ}\text{C}$  (Fig. 8). The middle fraction showed multiple peaks between 375 and  $500\,^{\circ}\text{C}$  that were best resolved at the higher sensitivity setting of  $S = 5$ . In the experiments with  $R = 4$ , an increase in *S* from 1 to 5 brought the light fraction to lower temperatures, but it decreased the resolution of the middle and heavy fractions as they came closer together (Fig. 9). The effect was much like that after a



decrease in a linear rate of heating (Fig. 6). Consequently, the best conditions for bitumen analysis by means of the dynamic rate method were with  $R = 3$  and  $S = 5$  (Fig. 8). These settings gave the greatest resolution of the various fractions.

#### *4.3. Constant reaction rate*

The dynamic rate method only led to a broad and often asymmetrical peak for the light fraction. The shape suggested the overlap of at least two mass loss steps. In an effort to improve the sharpness of the signal from the light fraction, or deconvolute the underlying processes, the experimental conditions were changed to allow for a constant rate of volatile gas evolution. This required negative *R*-values and a low maximum heat rate, selected at 5 ◦C/min. Fig. 10 shows the results for bitumen analyzed with  $S = 1$  and  $R = -2$  to  $-5$ . There was not much improvement in the profile of the light fraction with *R* at  $-2$  and  $-3$ , but with  $R = -4$  and  $-5$ , two partially resolved peaks were evident rather than a single broad one. Above  $350^{\circ}$ C, the DTG profile was a succession of heating



Fig. 8. Effect of *S* on the bitumen DTG profile after a dynamic rate experiment.

Fig. 10. Effect of *R* on the bitumen DTG profile after a constant reaction rate experiment.



Fig. 11. Effect of *S* on the bitumen DTG profile after a constant reaction rate experiment.

and cooling steps applied in an attempt to keep the rate of gas evolution constant at temperatures where bitumen is in its auto-ignition range [4]. The greatest control over the evolution of gases above 350 ◦C was obtained when *R* was −2, conditions under which no cooling was applied.

Building again on these results, the effect of a varying *S* and a const[ant](#page-7-0) *R* of −2 on the resolution of the middle and heavy fractions was investigated. Fig. 11 shows the results when *S* was 1 and 3. With  $S = 3$ , the middle fraction, between 350 and 450 ◦C, showed four peaks with relatively good resolution of the various signals. Poor resolution was obtained with  $S = 1$ .

# *4.4. Customized methods*

In reviewing the conditions investigated, it is obvious that one set of *R*- and *S*-values does not allow for the resolution of all bitumen fractions at all temperatures. The light fractions with a mass loss peak below 350 ℃ are best resolved under the conditions of a constant decomposition rate when *R* is −4 and *S* is 1 (Fig. 10). The middle fraction also shows a good resolution of its multiple peaks in this mode when  $R = -2$ and  $S = 3$  (Fig. 11), and in the dynamic rate mode when *R* is 3 and *S* is 5 (Fig. 8). In this latter mode, the heavy fractions [were](#page-4-0) [well](#page-4-0) resolved with an *R* of 3, regardless of the *S*-value (Fig. 8).

Given the above results, bitumen could be analyzed with a [good](#page-4-0) [re](#page-4-0)solution of its fractions under two sets of conditions (or two methods), both of which combine the constant reaction rate and dynamic rate conditions. With method-1 shown in Fig. 12, the conditions for a constant rate of reaction prevail from 170 to 440 ◦C with a change in *R* and *S* at 310 °C. After 440 °C, the dynamic rate conditions are used. With method-2 shown in Fig. 13, the conditions for a constant rate of reaction only prevail up to  $310^{\circ}$ C, after which dynamic rate conditions are used.

The analysis of bitumen by means of these methods provides a fingerprint in less than 2 h. The difference between bitumens of various sources will be shown later. With both



Fig. 12. Bitumen DTG profile after the application of method-1, the *R* and *S* settings being as indicated.

methods, the light fraction shows as a doublet of peaks not completely resolved, with a less intense peak being on the high-temperature side, and the heavy fraction shows as an intense peak near  $500\,^{\circ}$ C. The difference between the methods is mainly in the resolution of the middle fraction, which is heated under the conditions of a constant reaction with method-1, but heated under a dynamic rate in method-2. Given the extended temperature range where a constant reaction rate is found, method-1 might find an interesting application in the study of hydrocarbon degradation, especially as it relates to cracking and associated activation energies [25].

## *4.5. Reproducibility*

[T](#page-7-0)o ascertain that reproducibility in the results is achieved, it is best that the sample in the TG pan be of the same shape run after run. This is most easily achieved when the film is thin and flat. To get such a film, bitumen is pretreated so that it melts and flows to the bottom of the pan. For 5 mg of bitumen, 15 s at 170  $\degree$ C achieves the sought after results without a significant volatilization of material. Larger masses



Fig. 13. Bitumen DTG profile after the application of method-2, the *R* and *S* settings being as indicated.

Table 4



Fig. 14. Effect of the sample size on the DTG profile of the light fraction of the Petro-Canada bitumen.

of about 12 and 22 mg led to a loss of resolution from the light fraction, as a single mass loss peak was obtained rather than two (Fig. 14).

With a constant use of 5 mg of bitumen, the reproducibility in the profile of the light and heavy oils is excellent, with that between 350 and 450  $\degree$ C showing a slight variation, most likely because of imperfect control of bitumen auto-ignition at these temperatures (Fig. 15). The peak temperature for the heaviest fraction varied within about 5 °C, less than the difference between the peaks from different bitumens as will be seen shortly. The reproducibility in the mass loss at 325, 440 and 700 ◦C allows for the quantification of light, middle and heavy fractions in bitumen (Table 4). The standard deviation in the weight of the three fractions is better than 2%. Both the DTG profile and the content of the various fractions may be used to fingerprint the material.

## *4.6. Applications*

As stated in the introduction, it is often necessary to repeatedly use the same bitumen for the production of a bituminous



Fig. 15. Reproducibility of the DTG profile on five replicates of the Petro-Canada bitumen after method-1.

Weight of the various fractions in the Petro-Canada bitumen as per method-1

Replicate	Light	Middle	Heavy
	21.6	31.6	46.0
2	21.6	31.1	46.3
3	21.2	31.7	46.2
$\overline{4}$	21.7	31.6	45.6
5	21.0	30.5	47.6
Average Weight $(\sigma)$	21.4(0.3)	31.3(0.5)	46.3(0.8)
% deviation	1.4	1.6	1.7



Fig. 16. High-resolution DTG for bitumens of the same grade after method-1.

product of consistent characteristics. In practice, this is often done by the purchase of a given bitumen grade from a single supplier. QC/QA upon reception of the raw material may be done with method-1 or -2 detailed above and the results compared with those from previous shipments. A positive identification is easily done given that bitumens of the same grade, but of different crude sources, show different DTG profiles (Fig. 16). As expected, bitumens of different grades also show different profiles (Fig. 17). Hence, a bank of TG profiles may be built-up for the positive identification of any bitumen from a given process or source.



Fig. 17. High-resolution DTG for bitumens of different grades after method-1.

<span id="page-7-0"></span>

Fig. 18. High-resolution DTG for sealants after method-1.

The methods can also be applied to the analysis of endproducts. The case of bituminous crack sealants is illustrated in Fig. 18. Sealants contain a polymer, processing oils and a filler, in addition to bitumen [20]. The oils contribute to the light fraction and the polymer to the middle fraction. The filler shows as a weight loss beyond the heavy fraction, near 700 °C. The results of detailed work on sealants will be provided in another publication.

# **5. Conclusion**

Two high-resolution TG/DTG methods were developed by combining dynamic and constant reaction rate experiments. By applying the method, excellent resolution and reproducibility of about 10 mass loss steps were achieved with bitumen and bituminous sealants. These results indicate that the TG/DTG method may be used for QC/QA applications and for the fingerprinting of such materials. The method shows potential for other applications, some examples being the quantification of bitumen fractions and that of components in end-products, and the study of cracking processes in heavy hydrocarbons.

# **Acknowledgement**

The authors would like to thank Mr. Peter Collins for comments and suggestions during the preparation of the manuscript.

# **References**

- [1] D.R. Jones IV, SHRP materials reference library for asphalt cements: a concise data compilation. Report SHRP-A-645, Strategic Highway Research Program, National Research Council, Washington, DC, 1993.
- [2] J-F. Masson, P. Collins, G. Robertson, J.R. Woods, J. Margeson, Energy Fuels 17 (2003) 714.
- [3] J-F. Masson, T. Price, P. Collins, Energy Fuels 15 (2001) 955.
- [4] H.J. Völker, H. Fisher, Conf. Chem. Chem. Process Petrol. Natur. Gas, Budapest, 1965, pp. 650–656 (in German).
- [5] M. Wesołowski, Thermochim. Acta 46 (1981) 21.
- [6] Anonymous, Hazardous Materials, sixth ed., National Fire Protection Agency, 1975.
- [7] P.R. Herrington, G.F.A. Ball, J.E. Patrick, Thermochim. Acta 202 (1992) 201.
- [8] S.M. Dyszel, Thermochim. Acta 38 (1980) 299.
- [9] M. Václav, Hutn. Listy 23 (1968) 43 (in Slovak).
- [10] J. Rouquerol, Bull. Soc. Chim. (1964) 31 (in French).
- [11] J. Rouquerol, Thermochim. Acta 144 (1989) 209.
- [12] J. Paulik, F. Paulik, Anal. Chim. Acta 56 (1971) 328.
- [13] F. Paulik, J. Paulik, Thermochim. Acta 100 (1986) 23.
- [14] O.T. Sorensen, Thermochim. Acta 13 (1978) 429.
- [15] O.T. Sorensen, Proceedings of the fifth meeting of AICAT, AICAT, Trieste, 1983, p. 25.
- [16] W.J. Sichina, Am. Lab. 25 (1993) 45.
- [17] B.S. Crowe, R.S. Sauerbruun, United States Patent 5,165,792 (1992).
- [18] B.S. Crowe, R.S. Sauerbruun, United States Patent 5,368,391 (1994).
- [19] Anonymous, TA Instrument Operators Manual for Thermogravimetric Analyzer Q500, 2001, p. 30.
- [20] J-F. Masson, P. Collins, J. Margeson, G. Polomark, Transport. Res. Rec. 1795 (2002) 33.
- [21] J-F. Masson, L. Pelletier, P. Collins, J. Appl. Polym. Sci. 79 (2001) 1034.
- [22] J-F. Masson, P. Collins, P.-P. Légaré, Can. J. Civil Eng. 26 (1999) 395.
- [23] B. Verkoczy, K.N. Jha, J. Can. Petrol. Technol. 25 (1986) 47.
- [24] M.V. Kok, Thermochim. Acta 214 (1993) 315.
- [25] M.R. Gray, W.C. McCaffrey, Energy Fuels 16 (2002) 756.